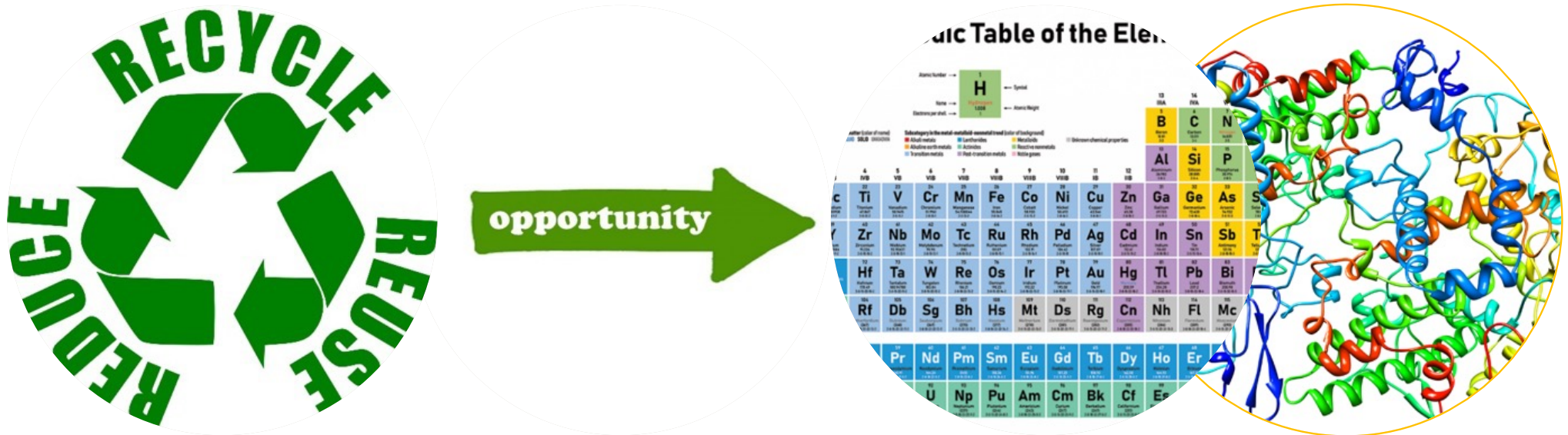


# (Bio)Chemical Recycling of Polycondensation Polymers

Depolymerization of polymer back to monomers: opportunities for chemicals & enzymes

Dr. Shanmugam Thiyagarajan, 14<sup>th</sup> October 2021  
Wageningen Food & Biobased Research, The Netherlands



# Wageningen University & Research



WU: 12,973 BSc/MSc-students; 2,196 PhD; 3,544 faculty and staff  
WR: 3,316 staff; Revenue in 2020: € 355 million

[www.wur.nl](http://www.wur.nl)

---

# Depolymerization potential of polymers

## ■ Polyolefins

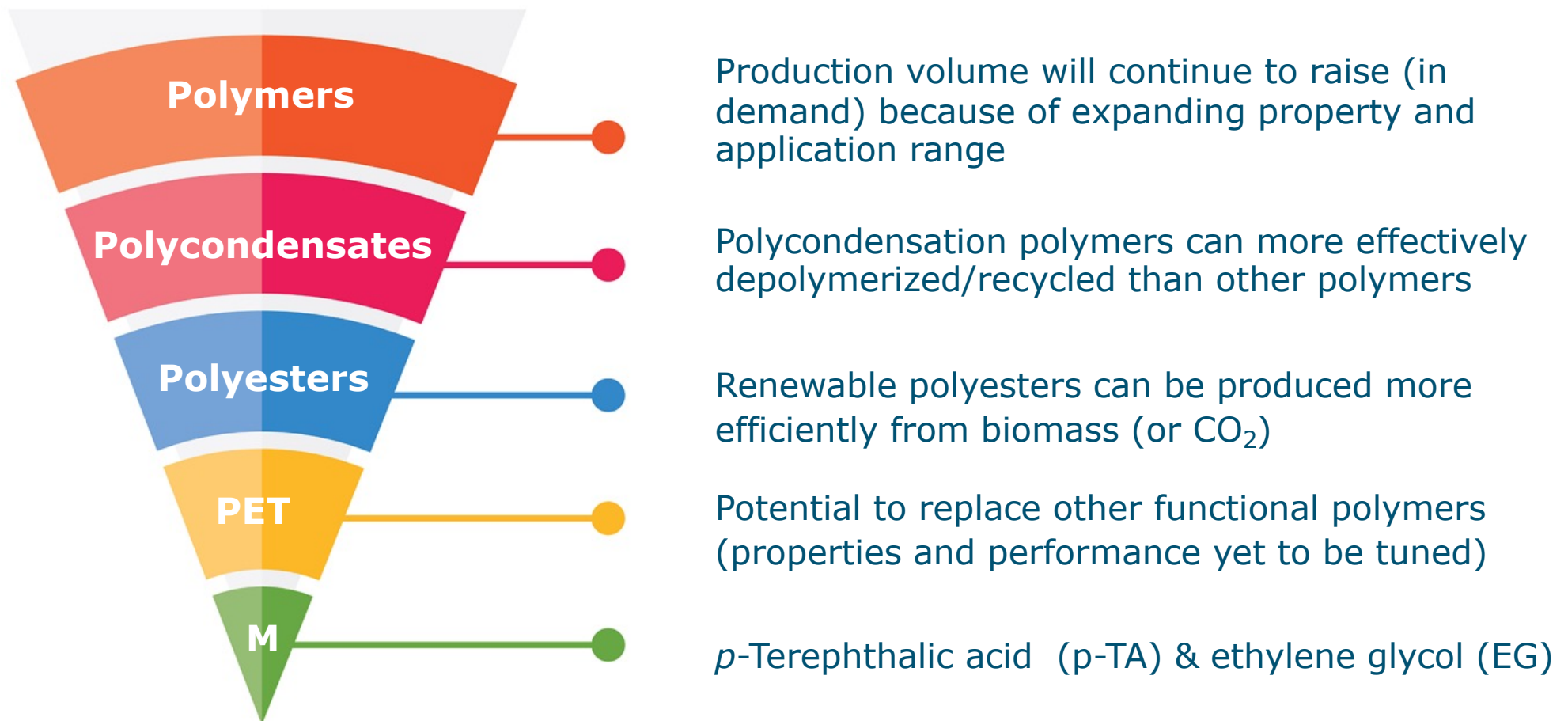
- Polyethylene (PE), Polypropylene (PP)...
- carbon-carbon (-C-C-) bonds are strong, harsh condition required to breakdown these polymers
- monomer recovery: difficult, often in lower percentages

## ■ Polycondensates

- Polyesters, Polyamides...
- ester (-COO-)/amide (-CONH-) bonds are labile, can breakdown at moderate conditions (comparatively)
- monomer recovery >90%, relatively in high selectivity

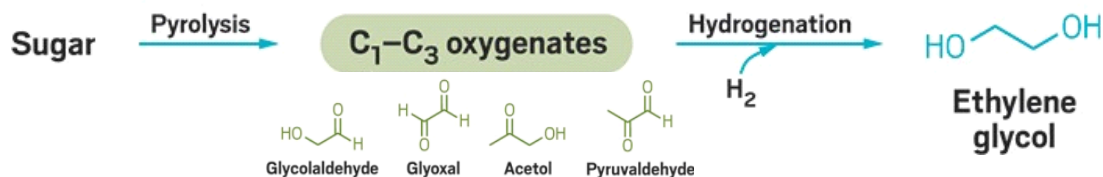


# Choice of polycondensation polymers



# EG (MEG) from biomass

## Haldor Topsoe process ( and Braskem)



## Conventional sugar-to-ethylene glycol approach

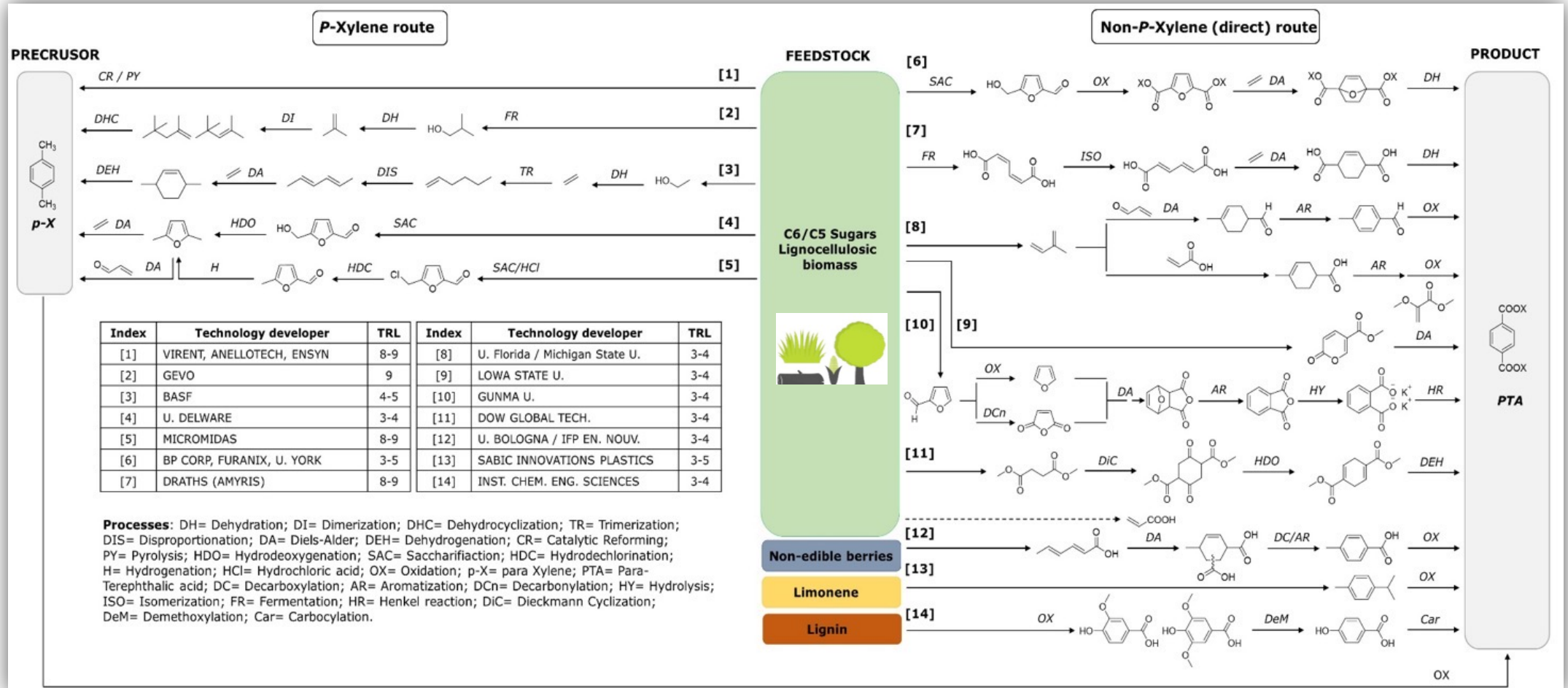


## Avantium Ray Technology

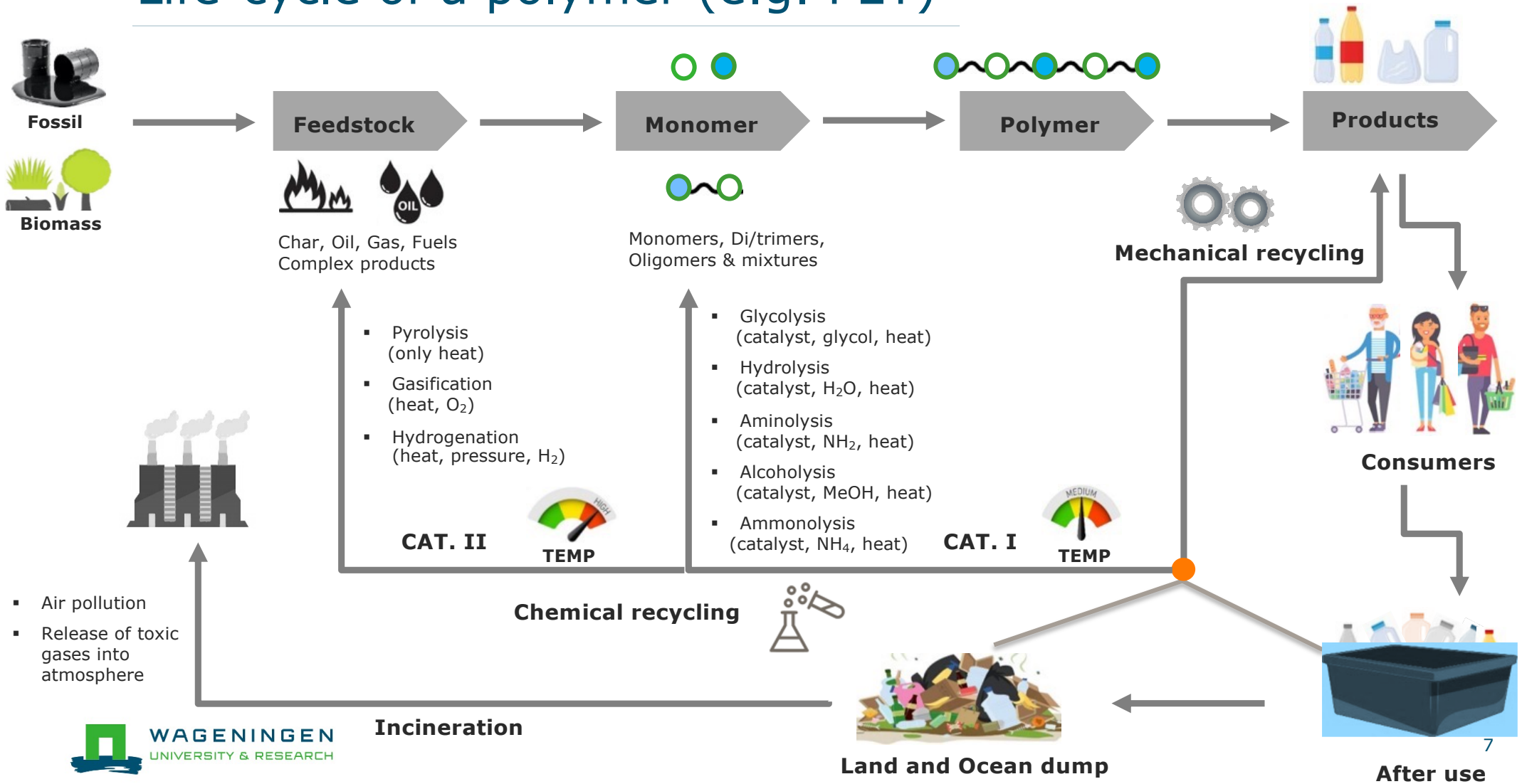
One-step hydrogenolysis process to produce MEG from plant-based sugars (maximum theoretical yield 100% and practical yield >70%)



# PTA from biomass



# Life-cycle of a polymer (e.g. PET)



---

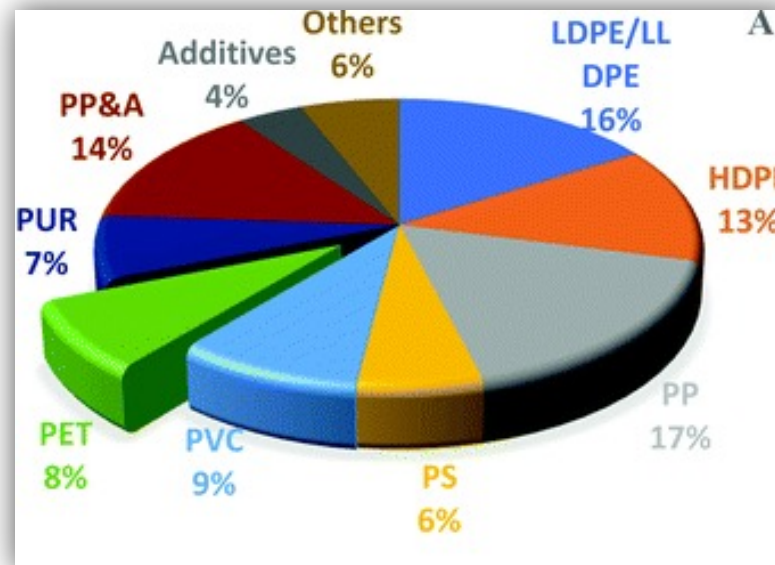
# Contents

- (Bio)-Chemical recycling of:
  - Polyesters >>> PET
- Processes includes:
  - Hydrolysis
  - Alcoholysis
  - Glycolysis
  - Aminolysis and Ammonolysis
  - Enzymatic hydrolysis
- Commercial status of chemical and enzymatic recycling technology



# Polyethylene terephthalate (PET)

- Global polymeric material production was 388 Mton in 2019
- Polyethylene terephthalate (PET) produced via polycondensation reaction
  - PET production volumes accounted for 8% (32 Mtons)



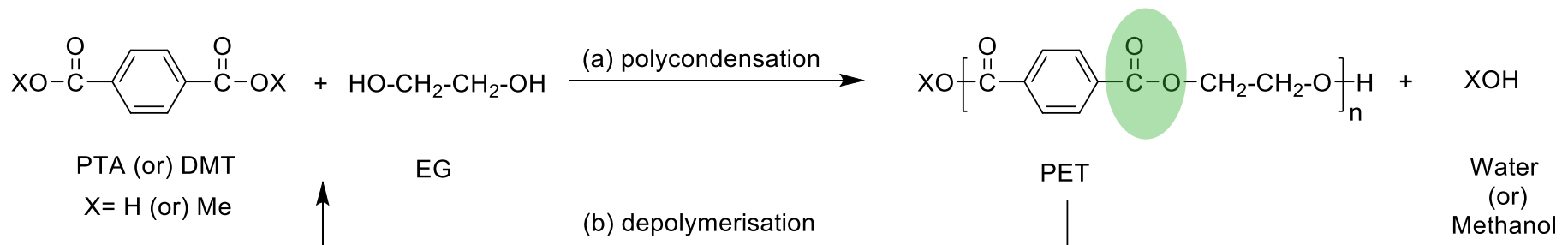
# Polyethylene terephthalate (PET)

- Polyethylene terephthalate (PET) received significant attention among various commercially available polyesters
  - Production: raw material available in larger volumes and inexpensive
  - Properties: high strength to weight ratio, transparency, durable
  - End of life: Potential for recycling
- Application areas includes (but not limited to) bottle, (food) packaging, and fabrics etc...



# Synthesis of Polyethylene terephthalate (PET)

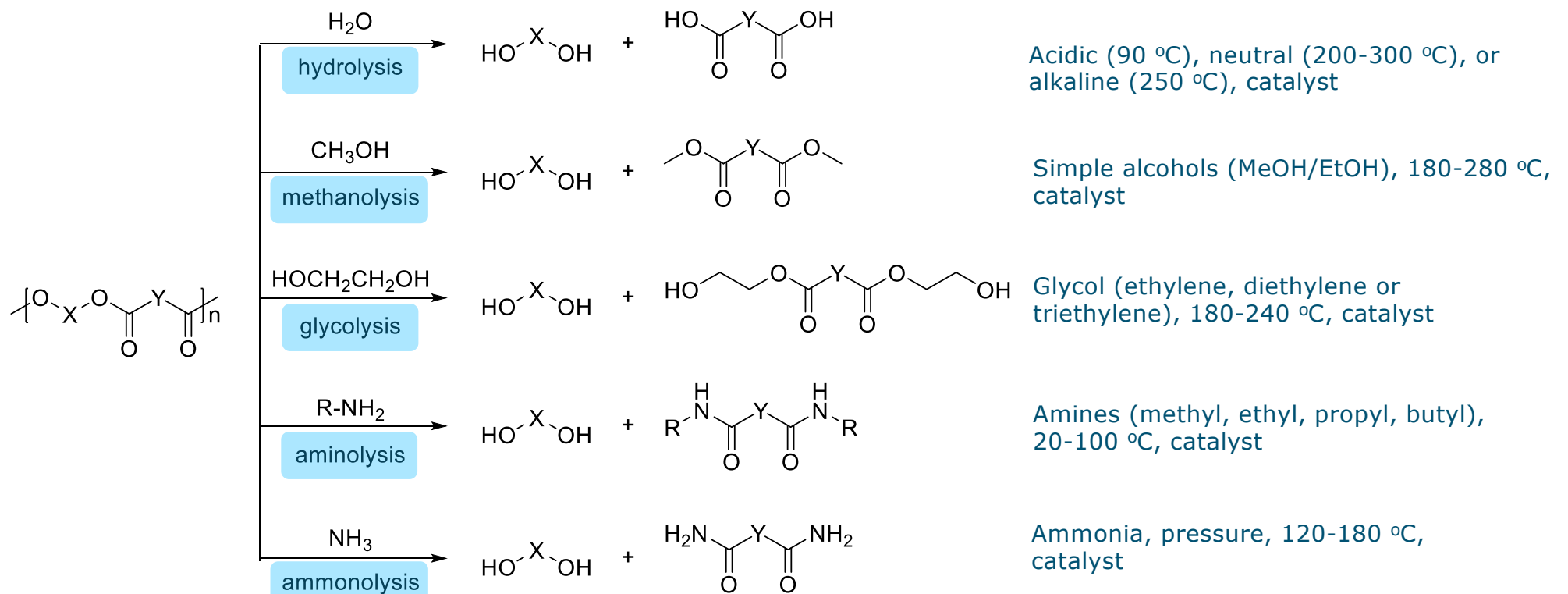
- Dimethyl terephthalate (DMT) (or) terephthalic acid (PTA) and ethylene glycol (EG) are the key monomers for PET production



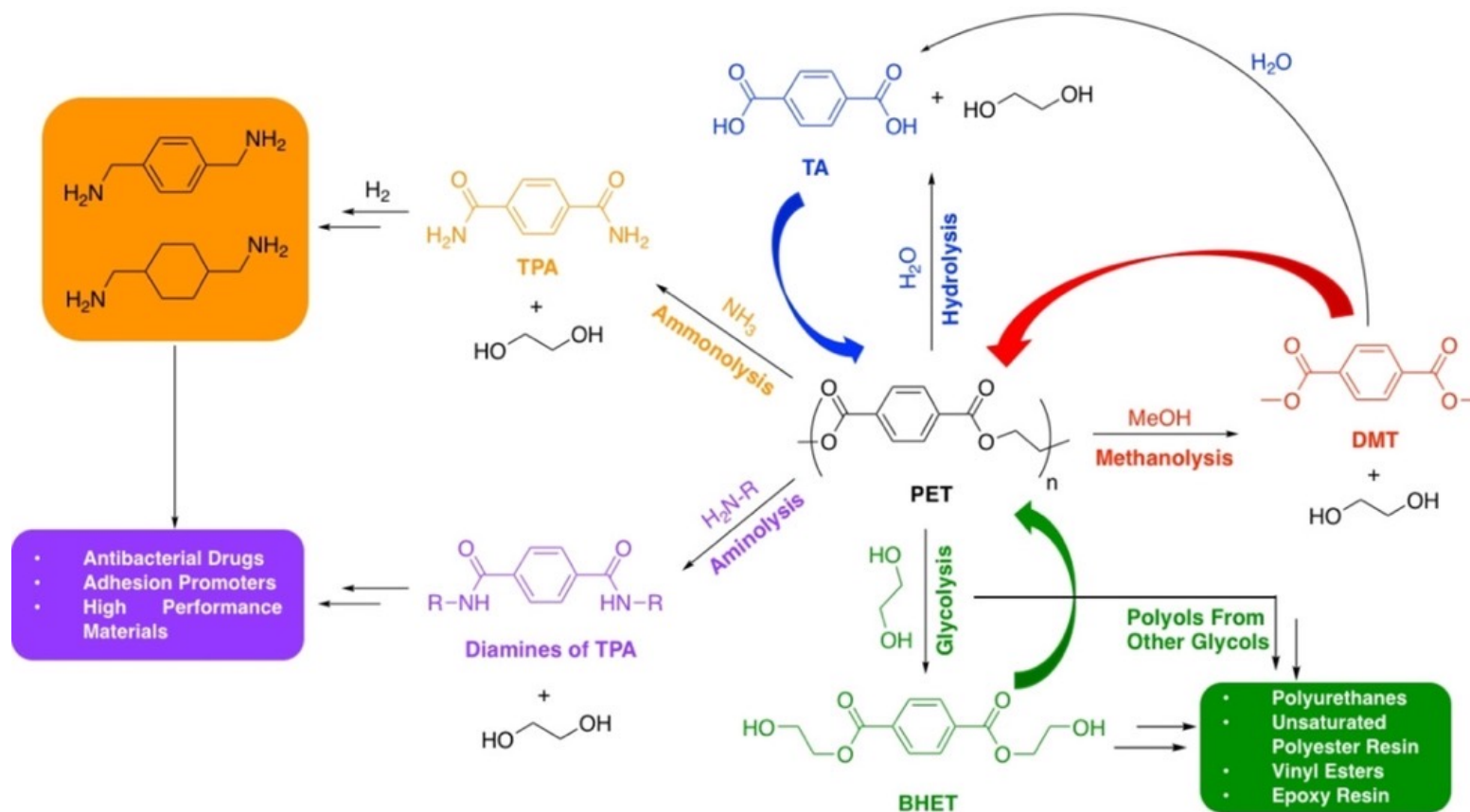
- (a) Condensation reaction between monomers in the presence of transesterification catalyst yields polymer
- (b) Ester bond in polyester offers opportunity to breakdown (suitable condition) resulting in starting monomers (and/or oligomers)

# Depolymerisation using solvolysis processes

- Solvolysis of PET demonstrated successfully using different solvents either presence/absence of catalyst

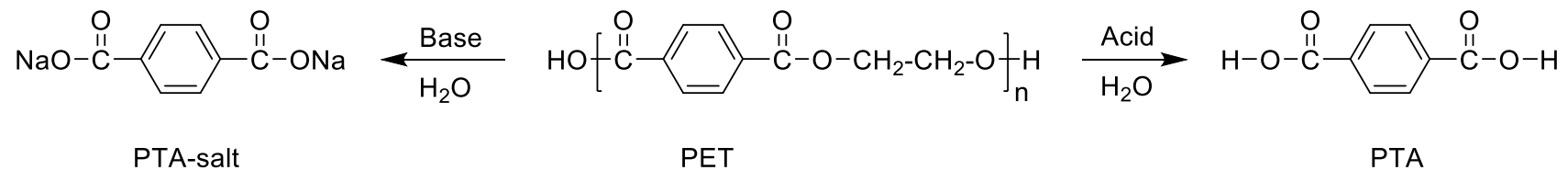


# Applications of products recycled from PET





# Hydrolysis (Acid, Base & Neutral) of PET



Type	Reagents	Catalyst
Acid	Sulfuric acid, Nitric acid, Phosphoric acid	None
Base	Sodium hydroxide, Potassium hydroxide	Trioctyl methylammonium bromide, Tetrabutyl ammonium bromide, Tetrabutyl ammonium iodide
Neutral	Water	Zinc/Sodium acetate, Hydrotalcite, Potassium hydroxide, Organophosphotungstic catalyst, zeolites

- Each process have their own merits and demerits depending on the operating conditions

# Hydrolysis (Acid, Base & Neutral) of PET

- Overview of selected conditions developed for efficient depolymerization of PET back to monomers

Technology developer	Starting material	Technology	Conditions						No. of steps <sup>1</sup>	Recovered		TRL <sup>2</sup>	Criteria <sup>3</sup>		
			Solvent	Reagent	Catalyst	Time (h)	Temp. (°C)	Pressure (bar)		Monomer <sup>4</sup>	Yield (%)		C <sup>5</sup>	P <sup>6</sup>	R <sup>7</sup>
Tohoku University - Japan	c-PET <sup>8</sup>	Acid Hydrolysis	H <sub>2</sub> O	Sulfuric acid	-	1-6	150	ATM <sup>9</sup>	1	PTA <sup>10</sup>	100	3-4	+/-	+	+/-
Aristotle University - Greece	c-PET <sup>8</sup>	Base Hydrolysis	H <sub>2</sub> O	Sodium Hydroxide	-	1-2	200	ATM <sup>9</sup>	2	PTA <sup>10</sup>	98	3-4	+/-	+	+/-
Al-Mustansiriyah University - Iraq	c-PET <sup>8</sup>	Base Hydrolysis	H <sub>2</sub> O	Sodium Hydroxide	Tetrabutyl ammonium bromide	1-2	200	ATM <sup>9</sup>	2	PTA <sup>10</sup>	98	3-4	+/-	+	+/-
NIAIST-Japan	PET <sup>11</sup>	Neutral Hydrolysis	H <sub>2</sub> O	H <sub>2</sub> O	-	0.5-1	420	480	1	PTA <sup>10</sup>	90	3-4	+	+	+
Zhejiang University of Technology - China	c-PET <sup>8</sup>	Netural Hydrolysis	H <sub>2</sub> O	H <sub>2</sub> O	Zn(OAc) <sub>2</sub>	0.5-1	220-300	32	1	PTA <sup>10</sup>	91	3-4	+	+	+/-

1. Number of steps to obtain final monomer back; 2. TRL: Technology readiness levels according to EU definitions, estimated by the authors based on publicly available information; 3. The symbols in the criteria section (estimated by the authors based on publicly available information) are defined as; +: high (or) attractive; -: low (or) less attractive; +/-: average (or) not convincing; 4. Type of monomer obtained from the process; 5. Reaction conditions and possible scale-up options; 6. Purity of monomer(s) obtained in the process; 7. Recycling/reusing possibilities of solvents/reagents/catalysts used in the process; 8. Commercial PET sample (Mn 30 Kda or higher); 9. Atmospheric pressure; 10. P-Terephthalic acid; 11. Post-consumer PET waste fraction (mixed PET fraction), pre-treated by extrusion to obtain amorphous PET.

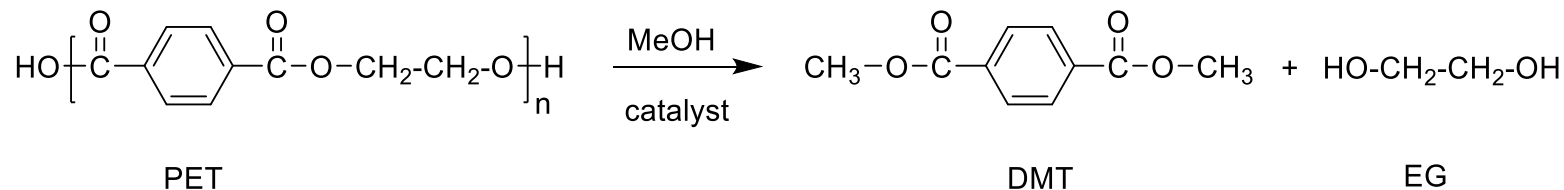
---

# Hydrolysis (Acid, Base & Neutral) of PET

---

- Though near quantitative yields achieved, some drawbacks that hampers large scale processes
- Acid hydrolysis
  - Severe corrosion of the reactors
  - Loss of recovered monomers (e.g. over oxd. of EG to Oxalic acid)
  - High costs for down-stream processing (DSP)
- Base hydrolysis
  - Often operated at higher T, Inorganic salts formation
  - High costs for down-stream processing (DSP)
- Neutral hydrolysis
  - Monomer (PTA) purity significantly low

# Alcoholysis of PET



- Directly yields monomers (DMT and EG), easily recovered by distillation, recrystallization/sublimation
- Organometallic catalysts (or) metal catalyst typically used<sup>1</sup>
  - $\text{Zn}(\text{OAc})_2$ ,  $\text{Mg}(\text{OAc})_2$ ,  $\text{Co}(\text{OAc})_2$ ,  $\text{Al}(\text{O-}i\text{-Pr})_3$ ,  $\text{PbO}_2$ ,  $\text{ZnO}$  (NPs)
- Ionic liquids ([Bmim]Cl) and DES (ChCl·ZnAc) were also demonstrated using supercritical ethanol and methanol
  - DMT yields achieved up to 97.7% at higher temperatures (>200 °C)

# Alcoholysis of PET

- Overview of selected conditions developed for efficient depolymerization of PET back to DMT and EG

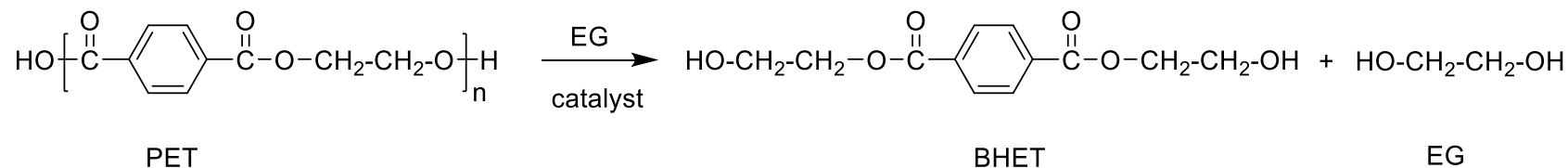
Technology developer	Starting material	Technology	Conditions						No. of steps <sup>1</sup>	Recovered		TRL <sup>2</sup>	Criteria <sup>3</sup>		
			Solvent	Reagent	Catalyst	Time (h)	Temp. (°C)	Pressure (bar)		Monomer <sup>4</sup>	Yield (%)		C <sup>5</sup>	P <sup>6</sup>	R <sup>7</sup>
Imam Khomeini Int. University - Iran	c-PET <sup>8</sup>	Alcoholysis	Butanol	Butanol	KOH	N.D. <sup>12</sup>	100	ATM <sup>9</sup>	2	PTA <sup>10</sup>	96	3-4	+/-	+	+/-
Imam Khomeini Int. University - Iran	c-PET <sup>8</sup>	Alcoholysis	Pentanol	Pentanol	KOH	N.D. <sup>12</sup>	100	ATM <sup>9</sup>	2	PTA <sup>10</sup>	96	3-4	+/-	+	+/-
Kumamoto University - Japan	c-PET <sup>8</sup>	Methanolysis	Methanol	Methanol	-	0-1.5	300	147	1	DMT <sup>13</sup>	98	3-4	+	+	+
Chinese Academy of Sciences- China	c-PET <sup>8</sup>	Methanolysis	Methanol	Methanol	Zn(OAc) <sub>2</sub>	0.5-1	250-270	110	1	DMT <sup>13</sup>	95	3-4	+	+	+/-

1. Number of steps to obtain final monomer back; 2. TRL: Technology readiness levels according to EU definitions, estimated by the authors based on publicly available information; 3. The symbols in the criteria section (estimated by the authors based on publicly available information) are defined as; +: high (or) attractive; -: low (or) less attractive; +/-: average (or) not convincing; 4. Type of monomer obtained from the process; 5. Reaction conditions and possible scale-up options; 6. Purity of monomer(s) obtained in the process; 7. Recycling/reusing possibilities of solvents/reagents/catalysts used in the process; 8. Commercial PET sample (Mn 30 Kda or higher); 9. Atmospheric pressure; 10. P-Terephthalic acid; 12. Not described; 13. Dimethyl terephthalate.



# Glycolysis of PET

- Process of depolymerizing PET chains using glycols at temperature between 180-240 °C



- BHET (α,ω-dihydroxy molecule) and glycolates obtained as end-product
  - BHET used as monomer for PET synthesis
  - Glycolates in unsaturated polyester resins, vinyl esters, plasticizers, polyurethanes and epoxy resin etc...

---

# Glycolysis of PET

---

- Glycols investigated
  - Ethylene glycol (EG), diethylene glycol (DEG), propylene glycol (PG), dipropylene glycol (DPG), 1,4-butanediol (BD)
  - Triethylene glycol (TEG), poly(ethylene glycol) neopentyl glycol (NPG)
- Catalysts explored: transesterification catalyst, metal salts, metal oxides, ionic liquids (acid, base and neutral), hydrotalcites, deep eutectic solvents (DES), zeolites, organic base, Polyoxometalates (POMs), Urea/metal salt mixtures, popular examples includes:
  - $\text{Zn}(\text{OAc})_2$ ,  $\text{Mn}(\text{OAc})_2$ ,  $\text{Co}(\text{OAc})_2$
  - $\text{NaHCO}_3$ ,  $\text{Na}_2\text{SO}_4$ ,  $\text{K}_2\text{SO}_4$ ,
  - Tetrabutoxy titanium, Titanium isopropoxide

# Glycolysis of PET

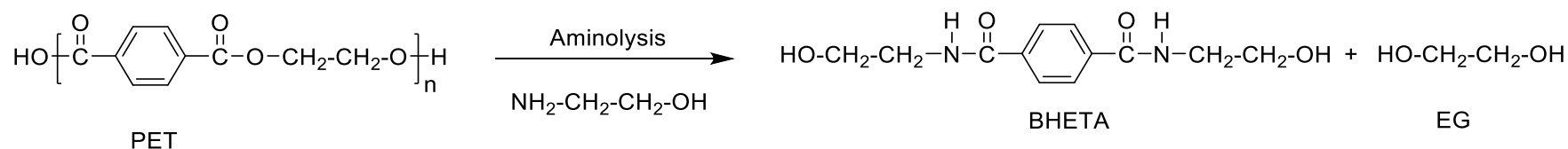
- Overview of selected conditions developed for efficient depolymerization of PET back to BHET monomer

Technology developer	Starting material	Technology	Conditions						No. of steps <sup>1</sup>	Recovered		TRL <sup>2</sup>	Criteria <sup>3</sup>		
			Solvent	Reagent	Catalyst	Time (h)	Temp. (°C)	Pressure (bar)		Monomer <sup>4</sup>	Yield (%)		C <sup>5</sup>	P <sup>6</sup>	R <sup>7</sup>
UFRGS-Brazil	c-PET <sup>8</sup>	Glycolysis	Ethylene glycol	Ethylene glycol	Zn(OAc) <sub>2</sub>	2	196	ATM <sup>9</sup>	1	BHET <sup>14</sup>	83	3-4	+	+	+/-
Henan Normal University - China	c-PET <sup>8</sup>	Glycolysis	Ethylene glycol	Ethylene glycol	Zn(OAc) <sub>2</sub>	1-5	196	ATM <sup>9</sup>	1	BHET <sup>14</sup>	86	3-4	+	+	+/-
Institute of Process Engineering -China	c-PET <sup>8</sup>	Glycolysis	Ethylene glycol	Ethylene glycol	Bmim <sub>2</sub> [CoCl <sub>4</sub> ]	1.5	175	ATM <sup>9</sup>	1	BHET <sup>14</sup>	96	3-4	+	+	+/-

1. Number of steps to obtain final monomer back; 2. TRL: Technology readiness levels according to EU definitions, estimated by the authors based on publicly available information; 3. The symbols in the criteria section (estimated by the authors based on publicly available information) are defined as; +: high (or) attractive; -: low (or) less attractive; +/-: average (or) not convincing; 4. Type of monomer obtained from the process; 5. Reaction conditions and possible scale-up options; 6. Purity of monomer(s) obtained in the process; 7. Recycling/reusing possibilities of solvents/reagents/catalysts used in the process; 8. Commercial PET sample (Mn 30 Kda or higher); 9. Atmospheric pressure; 10. P-Terephthalic acid; 12. Not described; 13. Dimethyl terephthalate; 14. Bis(2-hydroxyethyl) terephthalate.

# Aminolysis of PET

- Depolymerization of PET using amine solvent results in thermodynamically stable terephthalic acid amide



- Catalyst investigated

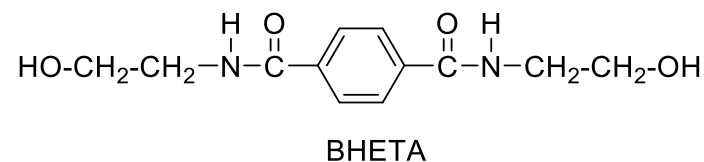
- Cetyl ammonium bromide (CAMBr), DBTO,  $\text{Zn}(\text{OAc})_2$ ,  $\text{Na}(\text{OAc})_2$ ,  $\text{K}_2\text{SO}_4$

- Solvents/Reagent

- Ethanol amine, methyl amine, diethanol amine, triethanol amine, ethylene diamine, triethylene tetra-amine, triethylene penta-amine

# Aminolysis of PET

- Potential application explored for BHETA includes:
  - novel polyurethanes, unsaturated polyester resins, bisoxazoline synthesis, and non-ionic polymeric surfactants
  - additives in concrete mixture
  - antibacterial chemicals

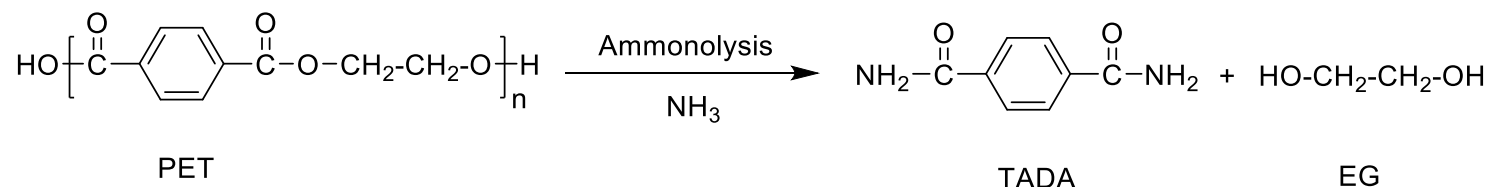


Technology developer	Starting material	Technology	Conditions						No. of steps <sup>1</sup>	Recovered		TRL <sup>2</sup>	Criteria <sup>3</sup>		
			Solvent	Reagent	Catalyst	Time (h)	Temp. (°C)	Pressure (bar)		Monomer <sub>4</sub>	Yield (%)		C <sup>5</sup>	P <sup>6</sup>	R <sup>7</sup>
Institute of Chemical Technology -India	C-PET <sup>8</sup>	Aminolysis	Acetic acid	Ethanol amine	Sodium acetate	0-0.5	172	ATM <sup>9</sup>	1	BHETA <sup>17</sup>	91	3-4	+/-	+	-



# Ammonolysis of PET

- PET depolymerization in the presence of ammonia at (higher) temperature is called ammonolysis

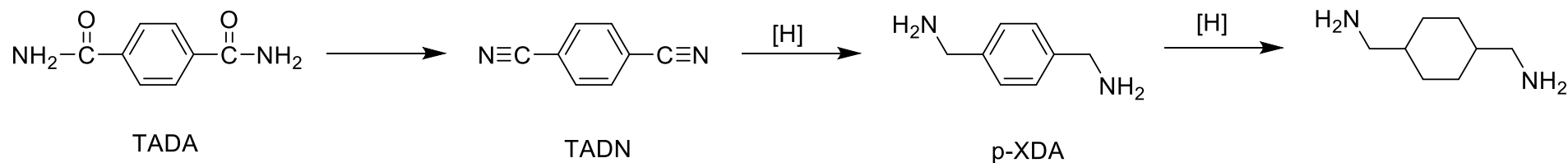


Technology developer	Starting material	Technology	Conditions							Recovered		TRL <sup>2</sup>	Criteria <sup>3</sup>		
			Solvent	Reagent	Catalyst	Time (h)	Temp. (°C)	Pressure (bar)	No. of steps <sup>1</sup>	Monomer <sub>4</sub>	Yield (%)		C <sup>5</sup>	P <sup>6</sup>	R <sup>7</sup>
Charan Singh University-India	c-PET <sup>8</sup>	Ammonolysis	-	NH <sub>4</sub>	Zn(OAc) <sub>2</sub>	360	RT <sup>18</sup>	ATM <sup>9</sup>	1	PTA diamide <sup>19</sup>	>90	3-4	+/-	+/-	-

- Operating conditions:
  - 70-180 °C, 2-20 bar NH<sub>3</sub>, Cetyl ammonium bromide (CAMBr), Zn(OAc)<sub>2</sub>

# Ammonolysis of PET

- Up to 90% terephthaldiamide (TADA) is obtained with >99% purity



- TADA can be used to produce terephthalonitrile (TADN), a precursor for either p-xylenediamine (p-XDA) or 1,4-bis(aminomethyl)cyclohexane, (for polyamide synthesis)

---

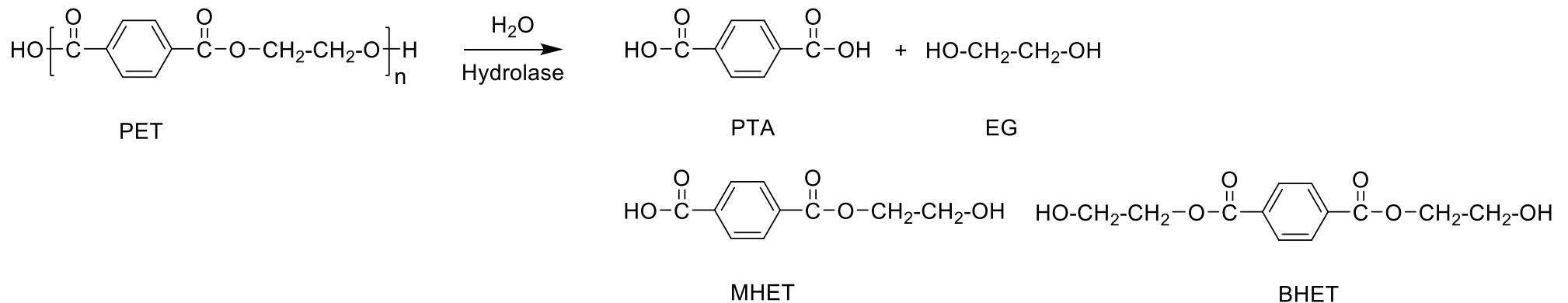
# Enzymatic hydrolysis of PET

---

- Enzymatic hydrolysis are advantageous
  - Environmentally friendly, mild reaction conditions (<100 °C); ATM pressure
- Amylases, cellulases, xylanases, pectinases, chitinases and cutinases are well-known examples of hydrolytic enzymes that breakdown naturally-occurring bio-polymers
- Lately, these enzymes proven for the depolymerisation of polycondensation polymers, for e.g. PET
- Carbios (French biotech company) front-runners in this technology, holding various patents and commercialized PET degradation using enzymes
- Main challenge: limited to amorphous or low-crystallinity materials (<10%)

# Enzymatic hydrolysis of PET

- Depending on enzyme and reaction conditions, one or more products are formed in typical enzymatic hydrolysis reaction



- MHET found to inhibit enzyme activity (*T-fusca* polyester hydrolase) and needs second enzyme addition to break down further to proceed the reaction

Type of Enzyme	Microorganism	Materials	Temperature (°C)	Product
Cbotu_EstA	<i>Clostridium botulinum</i> ATCC3502	PET film	50	TPA,MHET
Lipases	<i>Candida cylindracea</i>	PET nanoparticles	40	1,2-Ethandiol, TPA
Tcur0390	<i>Thermomonospora curvata</i> DSM43183	PET nanoparticles	50	NA
Hydrolase TtH	<i>Thermobifida fusca</i> DSM43793	PET pellete	44–55	TPA, EG
TtCut1	<i>Thermobifida fusca</i> KW3	PET nanospheres	55–65	HEB, MHET, BHET, Benzoic acid
Tha_Cut1	<i>Thermobifida alba</i> DSM43185	PET	50	TPA, Benzoic acid, HEB, MHET
MHETase and PETase	<i>Ideonella sakaiensis</i>	PET	30	MHET
BsEstB	<i>Bacillus subtilis</i> 4P3-11	PET	40–45	TPA, Benzoic acid, MHET
LCC cutinase	<i>Leaf-branch compost</i>	Amorphous PET	50–70	MHET, TPA, Benzoic acid
Polymer polyhydroxyalkanoate	<i>Pseudomonas</i>	PET	70	EG,TPA
Hydroxyalkanoyloxyalkanoate	<i>Pseudomonas</i>	PET	70	EG,TPA
Thc_Cut2	<i>T. cellulosilytica</i>	PET films	50	MHET, TPA, BA, HEB
Arg29Asn	<i>Mutant The_Cut2</i>	PET films	50	MHET, TPA, BA, HEB
Lipases	<i>Aspergillus oryzae</i> CCUG 33812	PET fabric	55	BHET,TPA
Gln65Glu	<i>Mutant The_Cut2</i>	PET films	50	MHET, TPA, BA, HEB
TtCut2	<i>Thermobifida fusca</i> KW3	PET films	60	MHET
Thh_Est-esterase	<i>Thermobifida halotolerans</i>	3PET model substrate	50	MHET,TPA, BA, HEB

## Overview of enzymatic degradation of PET

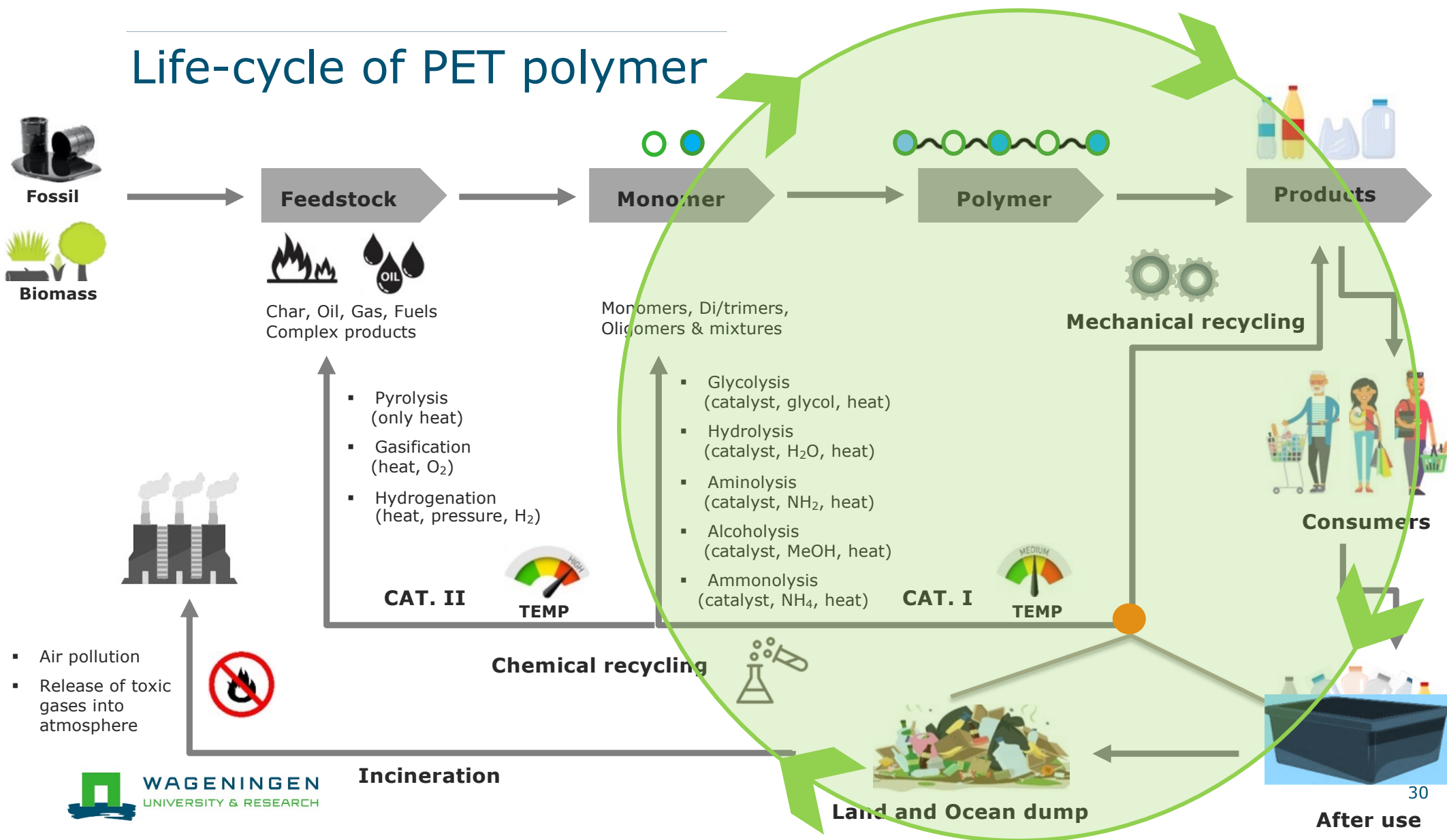
- Longer reaction time required for completion (10-96 h)
- Operated up to 70°C
- Various PET grades investigated
- Yield up to 97% demonstrated (mixture of monomers)



# Overview of chemical companies in PET recycling

Company	Type of PET plastic	Technology	Catalyst/Reagent/Medium	Monomer/product	Development stage	Processing capacity
Gr3n (DEMETO) - SW	Bottle grades, packaging, textile	Alkaline hydrolysis	Microwave, base	PTA <sup>1</sup>	Pilot plant	60 kg/h
Eastman	Bottle grade, <u>scrap from various products</u>	Glycolysis/ Methanolysis	N.I.A. <sup>2</sup>	BHET <sup>3</sup> /DMT <sup>4</sup>	Pilot plant	N.I.A. <sup>2</sup>
Loop	Low value material, fibre, carpet, scraps, <u>ocean debris</u>	Methanolysis	N.I.A. <sup>2</sup>	DMT <sup>4</sup>	Early commercial	N.I.A. <sup>2</sup>
IBM (VolCat) - USA	Bottle grade, packaging, scrap from various products	Glycolysis	DBU <sup>5</sup> (IBM)	BHET <sup>3</sup>	Early stage towards pilot plant	N.I.A. <sup>2</sup>
Garbo (ChemPET) - IT	Bottle grade, <u>multi-layer packages</u> , fibres, textiles	Glycolysis	N.I.A. <sup>2</sup>	BHET <sup>3</sup>	Pilot plant	1000 t/year
Ionika Technologies - NL	Bottle grades, <u>textiles</u> , multi-layer packages	Glycolysis	Magnetite, [Bmim][FeCl <sub>4</sub> ]	BHET <sup>3</sup>	commercial Pilot plant	10 kt/year
Jeplan (BRING)	Bottle grade, <u>fibre</u> , textiles	Glycolysis	Sodium Methylate, Carbon <sup>6</sup>	BHET <sup>3</sup>	Pilot plant	20-25 kt/year
PerPETual - UK/IN	Bottle grades	Glycolysis	N.I.A. <sup>2</sup>	Low MW oligomers	Commercial plant	~2 million plastic bottles per day
Resinate Materials Group (Recyolysis)	Bottle grade, scrap from various products, PETG	Glycolysis	N.I.A. <sup>2</sup>	Polyester Polyol <sup>7</sup>	Pilot plant	200 metric ton and 4,500 metric ton
Carbios - FR	Bottle grades, textile, fibres	Enzymatic	Engineered PET-depolymerase	PTA <sup>1</sup>	Pilot plant under construction	N.I.A. <sup>2</sup>
BP (Infinia)	Bottle, unrecyclable scrap from various products	Hydrolysis	N.I.A. <sup>2</sup>	PTA <sup>1</sup>	Early stage of Pilot plant	N.I.A. <sup>2</sup>
Poseidon Plastics	<u>Scrap from various products</u>	Glycolysis	N.I.A. <sup>2</sup>	BHET <sup>3</sup>	Pilot plant	1000 t/year

# Life-cycle of PET polymer



---

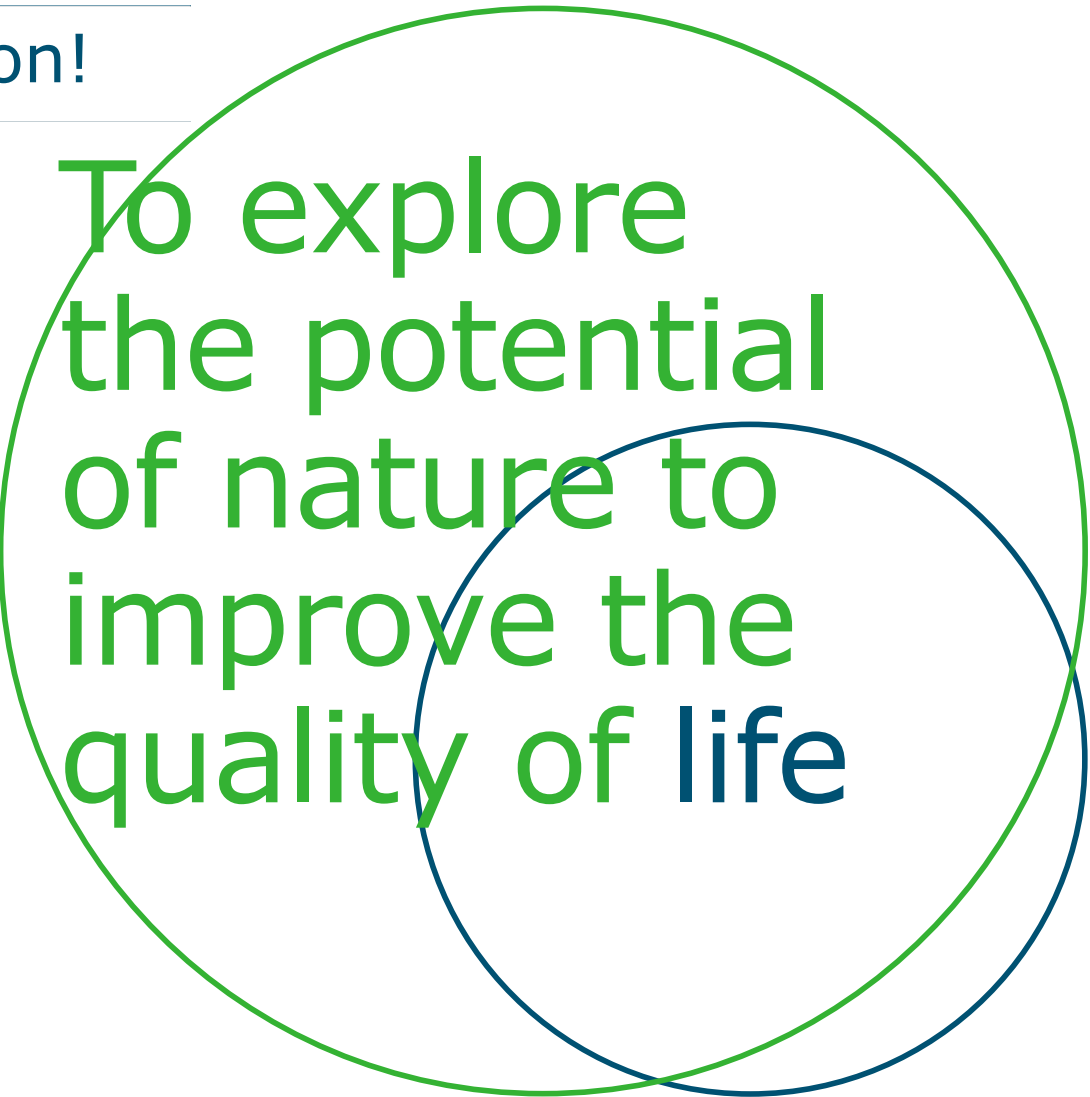
Thank you for your attention!

---

Acknowledgments: WFBR colleagues

[shanmugam.thiyagarajan@wur.nl](mailto:shanmugam.thiyagarajan@wur.nl)

+31-317-480158



To explore  
the potential  
of nature to  
improve the  
quality of life